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## Research Article AN INVESTIGATION OF GRINDING CHARACTERISTICS OF NA-FELDSPAR BY MEANS OF THE KINETIC MODEL PARAMETERS

# Serhan HANER\*<sup>1</sup>, Bülent HANER<sup>2</sup>, Tarık TUNAY<sup>3</sup>

<sup>1</sup>Süleyman Demirel University, Gönen Vocational School, ISPARTA <sup>2</sup>Bülent Ecevit University, Department of Mining and Mineral Extraction, ZONGULDAK <sup>3</sup>Süleyman Demirel University, Department of Mining Engineering, ISPARTA

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## ABSTRACT

In this study, the specific rates of breakage  $(S_i)$  and the primary breakage distribution  $(B_{i,j})$  values of Nafeldspar were determined for four mono-sized feed fractions; -0.106+0.090 mm, -0.090+0.075 mm, -0.075+0.063 mm, and -0.063+0.045 mm. Batch dry grinding tests were carried out for 0.25 and 0.50 minutes of grinding time by using labratory grinding mill having cylpebs with 10 mm diameter. And then the kinetic model parameters  $(S_i, a_T, \alpha, \gamma \text{ and } J)$  were calculated and presented in a comparative manner for different grinding times.

Keywords: Breakage parameters, cylpebs milling, kinetic model, na-feldspar.

## **1. INTRODUCTION**

The fine grinding in the micron range has recently become important in connection with the development of new functional materials such as new ceramics and electronic materials in various industrial fields. For grinding mills using spherical balls as grinding media, the effectiveness of small grinding balls on the fineness of ground products has been recognized as an important experimental factor [1-4].

The existence of a grinding limit is a problem that is inherent with fine grinding. Experimental study shows that particles that are larger than a certain limit experience breakage if subjected to enough intensive stress, while the smaller ones undergo plastic deformation only [5,6]. The nature of this phenomenon can be explained using concepts carried over from the physics of fracture.

Fine grinding is an intermediate case between coarse grinding and mechanical activation. Similar to coarse grinding, it is intended for size diminishing. However, it does not allow simple scaling because of its more complex physical background. Quantitative changes in particle size brings up qualitative changes in the nature of the process, so producing fine and ultrafine powders demands a more fundamental understanding of the physics of mechanical energy relaxation [7]. This circumstance makes fine grinding analogous to mechanical activation.

<sup>\*</sup> Corresponding Author/Sorumlu Yazar: e-mail/e-ileti: serhan.haner@gmail.com, tel: (246) 281 23 00

The analysis of s ize reduction in tumbling ball mills using the concepts of specific rate of breakage and primary daughter fragment distributions have received considerable attention in years. Austin et al. (1984) reviewed the advantages of this approach; and the scale-up of laboratory data to full-scale mills were discussed in a number of papers summarized by different researchers [8].

In this study, some problems concerning the relation between fine grinding and kinetic model parameters of the grinding time were explained. The main questions to be considered are the change of kinetic model parameters in fine size particles. In particular, how model parameters changed in fine particle size has not been demonstrated by researchers.

In this study, especially the breakage distribution function parameters were put forward in the fine particle sizes (-106+45  $\mu$ m). In addition, the Na-feldspar used in the study is also used in ceramic sanitaryware industry. Determining the grinding conditions of Na-feldspar and revealing the fragmentation characteristics will have contributions at industrial scale.

## 2. BACKGROUND

When breakage occurs in an efficient manner, the breakage of a given size fraction of material usually follows a first-order law [9]. Thus, the breakage rate of the material that is in the top size interval can be expressed as below:

$$\frac{-dw_1}{dt} = S_1 w_1(t) \tag{1}$$

Assuming that  $S_1$  does not change with time (that is, a first-order breakage process), this equation integrates to:

$$\log[w_1(t)] - \log[w_1(0)] = \frac{-S_1 t}{2.3}$$
<sup>(2)</sup>

where  $w_I(t)$  is the weight fraction of the mill hold-up of the size 1 at time t and  $S_I$  is the specific rate of breakage. The formula proposed by Austin et al. (1984) for the variation of the specific rate of breakage Si with grain size is:

$$S_i = a_T (X_i)^{\alpha} \tag{3}$$

where  $X_i$  is the upper limits of the size interval indexed by i (mm); and  $a_T$  and  $\alpha$  are the model parameters that depend on the properties of the material and the grinding conditions.

On breakage, grains of given size produce a set of primary daughter fragments, which are mixed into the bulk of the powder and then in turn have a probability of being re-fractured. The set of primary daughter fragments from breakage of size *j* can be represented by  $b_{i,j}$ , where  $b_{i,j}$  is the fraction of size *j* material, which appears in size *i* on primary fracture,  $n \ge i \ge j$ . It is convenient to represent these values in a cumulative form.

$$B_{i,j} = \sum_{k=n}^{i} b_{k,j} \tag{4}$$

Here,  $B_{i,j}$  is the sum fraction of the material less than the upper size of size interval *i* resulting from primary breakage of size *j* material:  $b_{i,j}=B_{i,j}$   $B_{i+1,j}$ . Austin et al. (1981) showed that the values of  $B_{i,j}$  could be estimated from a size analysis of the product from short time grinding of a starting mill charge predominantly in size *j* (the one-size fraction BII method) [10]. The equation is:

$$B_{i,j} = \frac{\log[(1-P_i(0))]/\log[(1-P_i(t))]}{\log[(1-P_{j+1}(0))]/\log[(1-P_{j+1}(t))]}, \qquad n \ge i \ge j+1$$
(5)

where  $P_i(t)$  is the fraction by weight in the mill charge less than size  $X_i$  at time t.  $B_{i,j}$  can be fitted to an empirical function [4].

$$B_{i,j} = \phi_j [X_{i-1}/X_j]^{\gamma} + (1 - \phi_j) [X_{i-1}/X_j]^{\beta} n \ge i \ge j$$
(6)

 $\phi_j = \phi_1 [X_i / X_1]^{-\delta} \tag{7}$ 

Here,  $\delta_i$ ,  $\gamma$  and  $\beta$  are the model parameters that depend on the properties of the material.  $\gamma$  is the slope of the lower section of the  $B_{i,j}$  curve; and  $\beta$  is the slope of the steeper section of the  $B_{i,j}$  curve as in Figure 1 [8,12].



Figure 1. Obtaining the primary breakage distribution function parameters for any single size fraction feed ground in the mill

## **3. MATERIALS AND METHOD**

Feldspar minerals are major commodities used in the production of glass and ceramics. In a significant proportion of feldspar ores, Na-Feldspar (albite; NaAlSi<sub>3</sub>O<sub>8</sub>) and K-feldspar (KAlSi<sub>3</sub>O<sub>8</sub>; microcline or orthoclase) exist in the same matrix, usually in quantities of about 3-5% Na<sub>2</sub>O and K<sub>2</sub>O.

Na-feldspar (Milas deposit in Turkey) were chosen as the feed mineral for this study. Na-feldspar was characterized with X-ray fluorescence (XRF) using Spectro equipment, model X-Lab 2000; X-ray diffraction (XRD) using Philips equipment, model X'Pert MPD, with radiation Cu-K $\alpha$  (45 kV/ 40 mA). The densities of Na-feldspar, measured by a pycnometer, are averaged as 2.58 g/cm<sup>3</sup> over three measurements and Bond work indexes ( $W_i$ ) of this material are 13.27 kWh/t, respectively. The Bond work index is determined by using the standard Bond test procedure for 0.106 mm test sieve size [8].

The breakage parameters were determined experimentally using one size fraction technique [11]. The size fractions chosen for tests were, -0.106+0.090, -0.090+0.075, -0.075+0.063 and -0.063+0.045 mm. For example, -0.106+0.090 mm denotes that 100% of the grains pass by weight at 0.106 mm size and 100% of grains remain at 0.090 mm. The standard set of grinding conditions used is shown in Table 1 for a laboratory mill with a 2650 cm<sup>3</sup> volume.

Mill	Diameter, D mm	150		
	Length, mm	150		
	Volume, cm <sup>3</sup>	2650		
	Critical $(N_c)^a$ , rpm	113		
	Operational ( $\emptyset_c=75\%$ ), rpm	84.75		
Mill charge	Quality	Cylpebs		
-	Diameter, d mm	10		
	Specific gravity, g/cm <sup>3</sup>	6.75		
	Ball filling volume, $J^{b}$	0.30		
Media charge	Sample	Na-feldspar		
	Specific gravity, g/cm <sup>3</sup>	2.58		
	Powder weight, g	656.53	820.66	
	Powder filling volume, $f_c^{c}$	0.096	0.120	
	Powder-ball loading ratio, $U^d$	0.80	1.00	

Table 1. Ball mill characteristics and test conditions

<sup>a</sup>  $\overline{N_c} = 42.3/\sqrt{D-d}$  (D, d in metres) <sup>b</sup>  $J = ((\text{mass of balls/ball density})/(\text{mill volume})) \times (1.0/0.6)$ 

<sup>c</sup>  $f_c = (\text{mass of powder/powder density})/(\text{mill volume})$ <sup>d</sup>  $U = f_c/0.4J$ 

## 4. RESULTS AND DISCUSSION

#### 4.1. Properties of Na-Feldspar

Table 2 presents the chemical composition of Na-feldspar. The amount of K<sub>2</sub>O, MgO and Fe<sub>2</sub>O<sub>3</sub> in the Na-feldspar was 0.36, 0.21 and 0.18 mass-%, respectively. As a result of XRD analysis, biotite was identified in the Na-feldspar (Figure 2), because it is known that K<sub>2</sub>O, MgO and Fe<sub>2</sub>O<sub>3</sub> are the components of biotite.

SiO <sub>2</sub>	$Al_2O_3$	Na <sub>2</sub> O	MgO	K <sub>2</sub> O	CaO	$Fe_2O_3$	TiO <sub>2</sub>	LOI	
69.84	18.07	10.30	0.21	0.36	0.56	0.18	0.17	0.31	

Table 2. Chemical composition of Na-feldspar

Figure 2 shows the X-ray diffraction patterns of Na-feldspar. Na-feldspar consists of albite [ICDD (01-089-6423)], quartz [ICDD (01-085-1054)] and biotite [ICDD (00-002-0057)]. The XRD result was confirmed by a chemical analysis.

#### 4.2. Determination of S parameters

The initial grinding results obey the first-order breakage form as in Eq. (3). When the values of S<sub>i</sub> are fitted to the expression; the  $a_T$  value is obtained by inserting a and  $x_i$ . Using Eq. (3),  $S_i$ ,  $a_T$ and  $\alpha$  were obtained for Na-feldspar and outlined in Table 3 as the breakage parameters to use for simulations of the product size distributions. In Figure 3, the  $a_T$  value is the specific rate of breakage at 1000  $\mu$ m grain size, and  $\alpha$  is the inclination of the breakage rate curve.

Variations in specific rates of breakage at different feed particle sizes for cylpebs grinding charges are shown in Figure 3. The specific rate of breakage increases up to -90+75 µm feed size, but above this size, fraction breakage rates decrease sharply for powder filling ratios. The particles have a slow specific rate of breakage. This was due to the efficiency of the largest feed sizes that were not nipped properly by the balls in the mill. This means the feed sizes larger than 90 µm will not be ground efficiently in this mill with these ball sizes.



Figure 2. X-ray diffraction patterns of Na-feldspar



Figure 3. Variation of S<sub>i</sub> values of Na-feldspar with particle size for the different

## 4.3. Breakage distribution functions

The values of B were determined from the size distributions at short grinding times (0.25 and 0.50 min) using the BII method, and are shown in Figure 4. The results showed a typical-

normalized behavior so that the progeny distribution did not depend on the feed grain size and the parameter  $\delta$  was zero. The kinetic model parameters are also given in Table 3. As the amount of  $_i$  and  $\gamma$  values decreases, the effective breakage decreases, and breaks very slowly in the undersize of original particle size at 0.50 min. The lower  $\gamma$  values and the fineness factor contribute more to the large parameter values of the finer size fractions, and thereby  $_i$  values pave the way for the coarser size fractions. The values of the coefficient  $_i$  are related to the coarse-end of the breakage distribution function and show the rapidity with which fractions close to the feed size pass to the smaller size interval.

It should be noted that wet grinding of size intervals of Na-feldspar followed the first-order breakage law with constant-normalized primary breakage distributions. In addition, this sample does not depend on the grain size of cumulative breakage distribution function. Grinding time increased while the  $_{i}$  value and  $\gamma$  value were decreased with increasing grinding time.



Figure 4. Cumulative breakage distribution functions for the different powder filling

$f_{c}(\%)$	U(%)	$a_T$	α	i 0.25	0.50	γ 0.25	0.50	β 0.25	0.50
0.096	0.80	1.24	1.61	0.827	0.514	4.021	3.763	10.050	9.734
0.120	1.00	0.90	1.58	0.796	0.493	4.085	3.124	13.234	8.321

Table 3. Characteristic breakage distribution functions of different grinding time

## 5. CONCLUSIONS

Kinetic model parameters for grain size below 106  $\mu$ m were determined for the Na-feldpar sample, which is used in ceramic industry. When the studies are evaluated, it is observed that the materials above the 106  $\mu$ m grain size were examined in them. With this study, it was understood that the  $B_{i,i}$  parameter values ( $\gamma$ ; 0.5-1.5,  $\beta$ ;2.5-5,  $\beta$ ;0.5-1) given in the literature is valid for materials that have grain size above 106  $\mu$ m.

When the  $a_T$  values are considered (shown by  $a_T$  parameters in Table 3), it is determined that they were obtained as 1.24 and 0.90. Here, it is observed that more efficient refraction occurs in low material filling ratio, i.e. the original part is reduced into sub-dimension more quickly.

 $\Phi_{j}$ ,  $\gamma$  and  $\beta$  model parameter values from mill operating conditions were calculated from relative particle size graphics for  $B_{i,j}$  values determined at different material filling ratios, and are given in Table 3. In both material filling ratios, the  $_{j}$  value decreased with the increasing grinding time, in other words, slower refraction occurred from top dimensions to a lower dimension. It is understood that the first refraction occurred in 0.25 minutes. It was determined that  $\gamma$  value was 3.763 and 3.124 at minute 0.50, in other words, fine material amount increased with the grinding time.

The primary breakage distribution functions of Na-feldspar were found to be normalized, which means that they are independent from the initial feed size in the case of cylpebs.

Grinding results of Na-feldspar showed that Na-feldspar does not obey first-order breakage kinetics law in the case of cylpebs. The specific rate of breakage values,  $S_i$ , increased up to 90  $\mu$ m and then decreased sharply. This can be explained by the fact that fine particles are difficult to break and grind by the medium, and hence, the grinding efficiency decreased.

With this study, the number of the experiments will be decreased in various studies, the grinding circuit performance will be solved, the grinding costs will be decreased and the parameters that affect the grinding will be examined with more ease.

## NOMENCLATURE

 $a_T$  model parameter

 $B_{i,j}$  cumulative breakage distribution function Greek symbols  $\alpha$  model parameter  $\beta$  model parameter  $\gamma$  model parameter  $\Lambda$  model parameter  $\mu$  grain size at which correction factor is 0.5

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